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Linear Superposition: Tutorial on Thermal-RC Networks
Transient Analysis in Linear Thermal Systems

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Packaging Technology Development
Thermal/Mechanical Characterization

• 2014 Jan 29

Outline

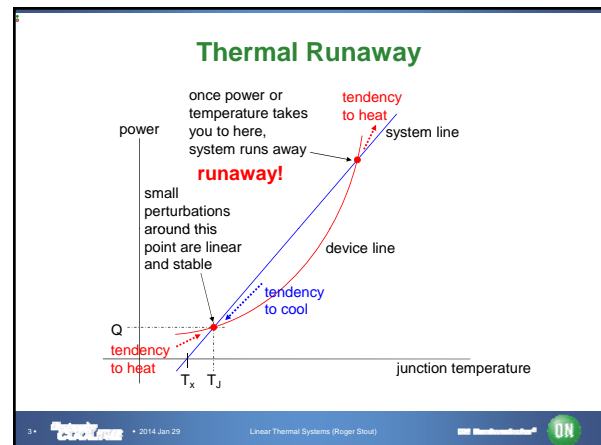
- Linear Systems fundamentals
 - why
 - what
 - some useful consequences
 - linear superposition
 - reciprocity
- Thermal RC Networks
- Case study – Calibration Chamber
 - design
 - step response experiments
 - fitting to measured data
 - predicting control input
 - testing predictions

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Linear Systems - why

- Why?
 - Because they can be analyzed!
 - frequency domain, modal analysis
 - time domain, s-plane, Laplace Transforms
 - Many real systems are sufficiently linear (meaning, over a useful range) that it's worth the effort
- Danger
 - If you forget, in the end, that you *assumed* linearity, you can go way wrong
 - thermal runaway provides a specific example

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 - Many real systems are sufficiently linear (meaning, over a useful range) that it's worth the effort
- Danger
 - If you forget, in the end, that you *assumed* linearity, you can go way wrong
 - thermal runaway provides a specific example
 - always prudent to review the range of the results to be sure you haven't gone too far outside the linear window, and what the implications might be

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Linear Systems – what

- Changes in the output variables are *proportional* to changes in the input variables

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Outputs Proportional to Inputs

$$\Delta T_1 = a_{11} \cdot q_1 + a_{12} \cdot q_2 + \cdots + a_{1n} \cdot q_n$$

$$\Delta T_2 = a_{21} \cdot q_1 + a_{22} \cdot q_2 + \cdots + a_{2n} \cdot q_n$$

⋮

$$\Delta T_m = a_{m1} \cdot q_1 + a_{m2} \cdot q_2 + \cdots + a_{mn} \cdot q_n$$

Linear Systems – what

- Changes in the output variables are *proportional* to changes in the input variables
- When time is considered, governing differential equations are linear

Governing Differential Equations are Linear

$$k_x \frac{\partial^2 T}{\partial x^2} + k_y \frac{\partial^2 T}{\partial y^2} + k_z \frac{\partial^2 T}{\partial z^2} = \rho c_p \frac{\partial T}{\partial t}$$

$$q = hA \cdot (T - T_A)$$

$$C_{th} \frac{dT}{dt} = q + \frac{T - T_A}{R_{th}}$$

Linear Systems – what

- Changes in the output variables are *proportional* to changes in the input variables
- When time is considered, governing differential equations are linear
- In the thermal domain
 - these are *constant*:
 - thermal conductivity
 - heat capacity
 - density
 - convection film coefficients

Coefficients are *constant*

$$k_x \frac{\partial^2 T}{\partial x^2} + k_y \frac{\partial^2 T}{\partial y^2} + k_z \frac{\partial^2 T}{\partial z^2} = \rho c_p \frac{\partial T}{\partial t}$$

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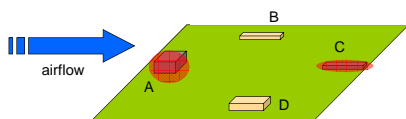
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Linear Systems – what

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 - thermal conductivity
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 - density
 - convection film coefficients
 - these restrictions generally apply:
 - convection is in algebraic proportion to temperature differences

Non-symmetric convection

- Upwind and downwind in forced-convection dominated applications



Heat in at "A" will raise temperature of "C" more than heat in at "C" will raise temperature of "A"

Linear Systems – what

- Changes in the output variables are *proportional* to changes in the input variables
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- In the thermal domain
 - these are *constant*:
 - thermal conductivity
 - heat capacity
 - density
 - convection film coefficients
 - these restrictions generally apply:
 - convection is in algebraic proportion to temperature differences
- radiation and free convection are inherently non-linear**

Radiation Resistance

basic heat transfer relationship for surface radiation is 4th-order in temperature, so

$$R = \frac{1}{\sigma \epsilon F A (T^2 + T_a^2)(T + T_a)} \quad \text{obviously not really a constant}$$

Free Convection

$$R = \frac{1}{hA} \quad \text{not explicitly temperature dependent, but } h, \text{ the film coefficient, depends on density, which is highly temperature dependent}$$

Poll Question #1

- Which of the following are intrinsically non-linear ...
 - Conduction heat transfer
 - Free convection heat transfer
 - Forced convection heat transfer
 - Radiation heat transfer

(choose all that apply)

Linear System Consequences

- If outputs are proportional to inputs, then the *inverse* problem (exchanging roles of inputs and outputs) is also linear

Role reversal

- Temperature can be the output, and power the input

$$T_j = \theta_{jx} \cdot q - T_x$$

- or, power can be the result, and temperature the input

$$q = \frac{1}{\theta_{jx}} \cdot T_j - \frac{T_x}{\theta_{jx}}$$

- either way, it's a linear equation

Linear Algebra Matrix Equivalent

- Temperature can be the output, and power the input

$$\bar{T}_j = [\theta_{jx}] \cdot \bar{q} + \bar{T}_x$$

- or, power can be the result, and temperature the input

$$\bar{q} = [\theta_{jx}]^{-1} \cdot \bar{T}_j - [\theta_{jx}]^{-1} \cdot \bar{T}_x$$

- either way, it's a linear equation

Linear System Consequences

- If outputs are proportional to inputs, then the *inverse* problem (exchanging roles of inputs and outputs) is also linear
 - In thermal systems, you can think of temperature as an output and power (heat) as the input, or you can think of temperature as the input and heat flow (power) as the output; either way, the problem is linear
- Linear superposition
 - solutions to particular cases can be linearly combined to create solutions to other cases

Linear superposition – what is it?

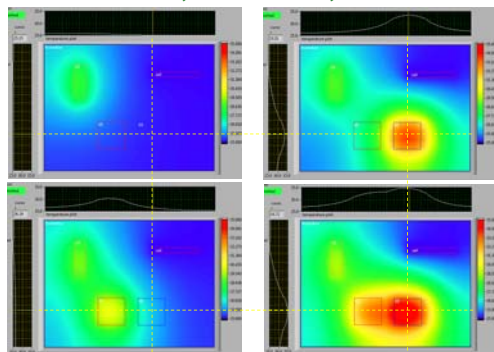
- The total response of a point within the system, to excitations at all points of the system, is the sum of the individual responses to each excitation taken independently.

$$\Delta T_{\text{composite}} = \Delta T_{\text{source 1}} + \Delta T_{\text{source 2}} + \dots + \Delta T_{\text{source n}}$$

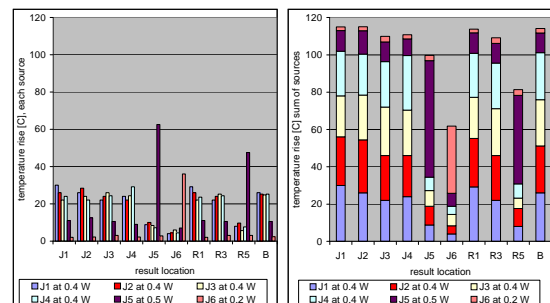
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- Linear superposition
 - solutions to particular cases can be linearly combined to create solutions to other cases
 - applies both spatially and temporally

U1=0.16 W, U2=0.30 W; U3=0.10 W



Bar Charts and Stacked Bar Charts (linear superposition visualized in Excel)



Linear System Consequences

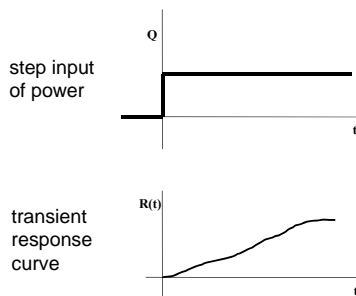
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- **Linear superposition**
 - solutions to particular cases can be linearly combined to create solutions to other cases
 - applies both spatially **and temporally**

Linear Superposition - temporally

- The combined response of a point to multiple independent time-varying inputs is the sum of the transient response of each individual time-varying input

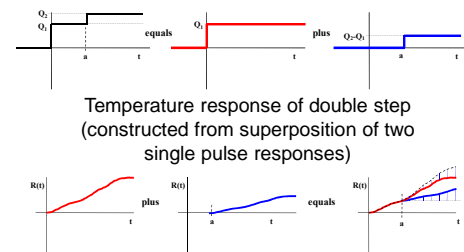
$$\Delta T(f_1(t), f_2(t) \dots f_n(t)) = \Delta T(f_1(t)) + \Delta T(f_2(t)) + \dots + \Delta T(f_n(t))$$

Basic Heating Curve - a "Single Pulse"



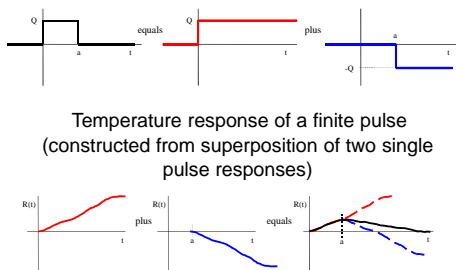
Double Step

double step, decomposed into two single steps



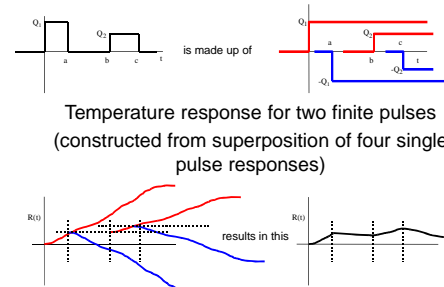
Single Square Pulse

Finite pulse, decomposed into two infinite steps



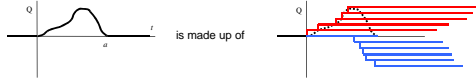
Two Differing Pulses

Two finite pulses decomposed into infinite steps

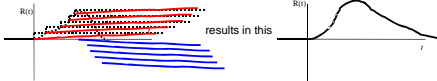


An Arbitrary Pulse

An arbitrary pulse decomposed into several infinite steps



Temperature response constructed for this arbitrary pulse

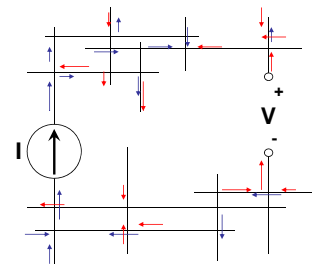


Linear System Consequences

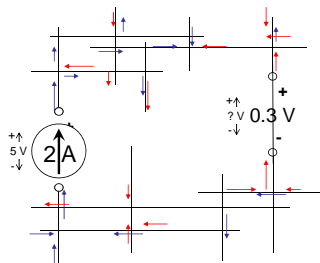
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- Linear superposition
 - solutions to particular cases can be linearly combined to create solutions to other cases
 - applies both spatially and temporally
- Reciprocity
 - a particular sort of mathematical symmetry that arises in fully linear systems

The Reciprocity Theorem

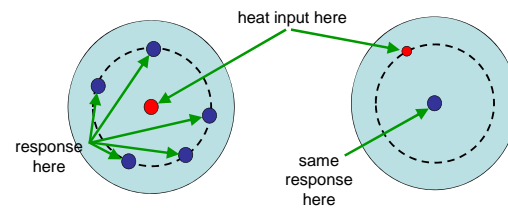
Electrical Reciprocity



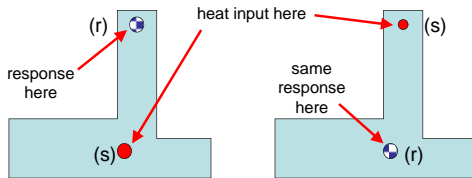
Electrical Reciprocity



Thermal Reciprocity



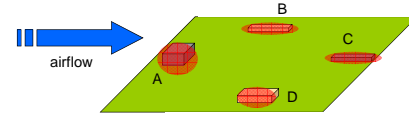
Another Thermal Reciprocity Example



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When Does Reciprocity NOT Apply?

- Upwind and downwind in forced-convection dominated applications



Heat in at "A" will raise temperature of "C" more than heat in at "C" will raise temperature of "A"

"B" and "D" may still be roughly reciprocal

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(Square part of) Matrix is Symmetric

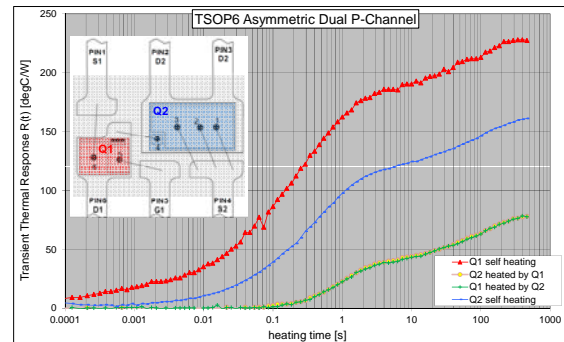
columns are the "n" heat sources

rows are the "m" response locations

J1	75	65	55	60	22	10
J2	65	71	60	55	25	11
J3	55	60	65	61	21	15
J4	60	55	61	73	18	11
J5	22	25	21	18	125	14
J6	10	11	15	11	14	180
R1	73	65	55	59	22	10
R3	55	60	63	61	21	15
R5	20	24	14	19	95	15
B	65	63	62	63	21	12

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Transient Reciprocity



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Poll Question #2

- Reciprocity ...
 - Relates temperature inputs and temperature responses
 - Is a covert CIA program to take out drug cartels
 - Relates heat inputs and temperature responses
 - Never applies to linear systems

(choose all that apply)

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- Thermal RC Networks**
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Thermal RC Networks

- Thermal/Electrical analogy
- Grounded vs. Non-grounded
 - physical significance
 - mathematical convenience
 - interchangeability
- 1-rung model(s)
- 2-rung models
 - "tau" is not RC product except when ...

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Thermal / Electrical Analogy

temperature	<=>	voltage
power	<=>	current
temp/power	<=>	resistance
energy/degree	<=>	capacitance

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Conduction Resistance

basic heat transfer relationship for 1-D conduction

$$q = k \cdot A \cdot \frac{dT}{dx} \approx k \cdot A \cdot \frac{\Delta T}{L}$$

if we define

$$R = \frac{\Delta T}{q}$$

then

$$R = \frac{L}{k \cdot A}$$

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Convection Resistance

basic heat transfer relationship for surface cooling

$$q = h \cdot A \cdot \Delta T$$

if we define

$$R = \frac{\Delta T}{q}$$

then

$$R = \frac{1}{hA}$$

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Radiation resistance

basic heat transfer relationship for surface radiation

$$\begin{aligned} q &= \sigma \cdot \varepsilon \cdot F \cdot A \cdot (T^4 - T_a^4) \\ &= \sigma \varepsilon F A (T^2 + T_a^2) \cdot (T^2 - T_a^2) \\ &= \sigma \varepsilon F A (T^2 + T_a^2) (T + T_a) \cdot (T - T_a) \\ &= \sigma \varepsilon F A (T^2 + T_a^2) (T + T_a) \cdot \Delta T \end{aligned}$$

if we define

$$R = \frac{\Delta T}{q}$$

then

$$R = \frac{1}{\sigma \varepsilon F A (T^2 + T_a^2) (T + T_a)}$$

obviously not
really a constant

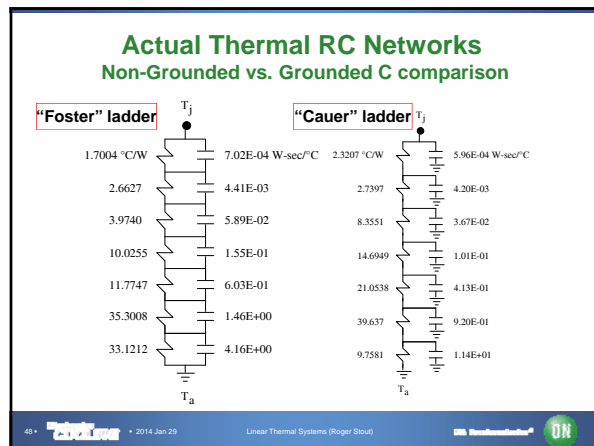
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Models: Grounded vs. Non-Grounded

("Cauer" ladders) ("Foster" ladders)

- Physical significance: if thermal capacitors are grounded, they bear some relationship to a physical system; not so for non-grounded C's
- Mathematical convenience: certain non-grounded networks (ladders) are mathematically trivial
- Interchangeability: single-input thermal systems can be represented as either grounded or non-grounded

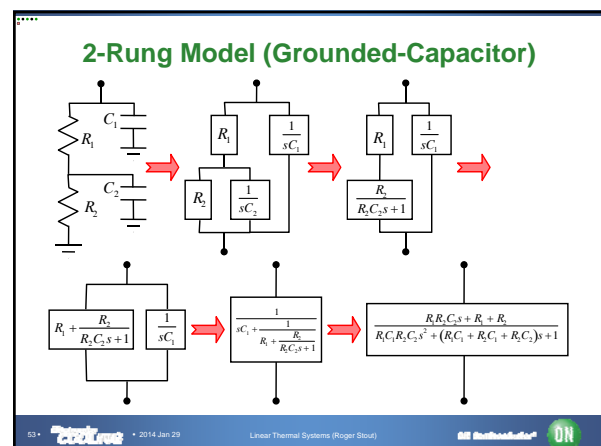
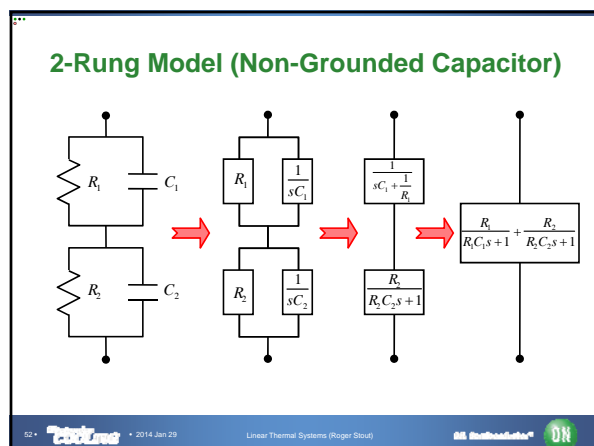
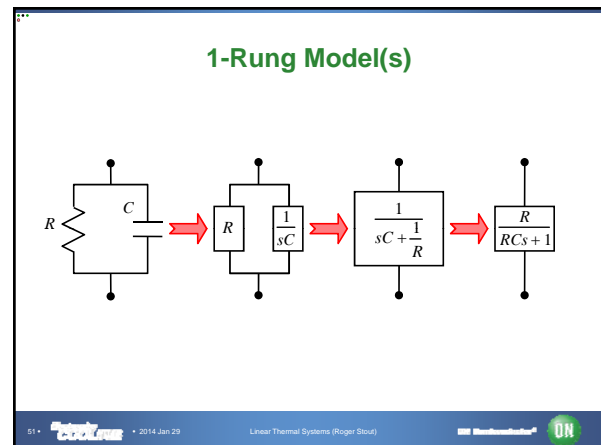
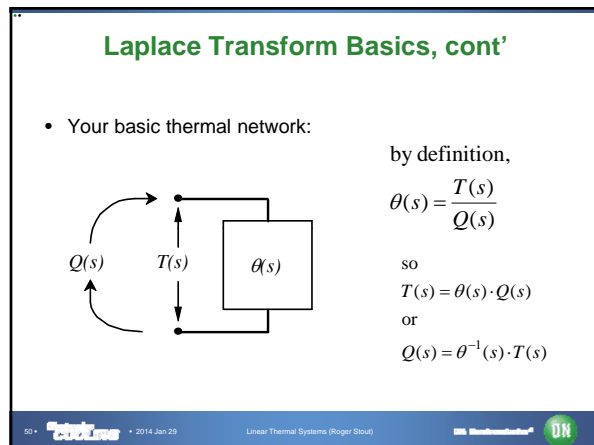
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Laplace Transform Basics

Item	time domain	s-plane	frequency domain
function	$f(t)$	$F(s) = \int_0^\infty e^{-st} f(t) dt$	
derivative	$\frac{df}{dt}$	$sF(s) - f(0)$	
resistor	$v = Ri$	$Z_R = R$	$Z_R = R$
capacitor	$i = C \frac{dv}{dt}$	$Z_C = \frac{1}{sC}$	$Z_C = \frac{1}{j\omega C}$
inductor	$v = L \frac{di}{dt}$	$Z_L = sL$	$Z_L = j\omega L$
exponential	e^{-at}	$\frac{1}{s+a}$	

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Compare the Transfer Functions

From the non-grounded-capacitor model

$$\frac{R_1}{R_1 C_1 s + 1} + \frac{R_2}{R_2 C_2 s + 1} = \frac{(C_1 + C_2) R_1 R_2 s + (R_1 + R_2)}{R_1 C_1 R_2 C_2 s^2 + (R_1 C_1 + R_2 C_2) s + 1}$$

From the grounded-capacitor model:

$$\frac{R_1 R_2 C_2 s + (R_1 + R_2)}{R_1 C_1 R_2 C_2 s^2 + (R_1 C_1 + R_2 C_1 + R_2 C_2) s + 1}$$

2-Rung Models Compared

- Time constants are roots of denominators
- "tau" is not RC product when capacitors are grounded!

non-grounded capacitors:
(Foster)

$$\frac{R_1}{R_1 C_1 s + 1} + \frac{R_2}{R_2 C_2 s + 1}$$

can be written

$$\frac{1}{C_1 s + \frac{1}{R_1}} + \frac{1}{C_2 s + \frac{1}{R_2}}$$

where time constants are
 $\tau_1 = R_1 C_1$ $\tau_2 = R_2 C_2$

grounded-capacitors: (Cauer)

$$\frac{R_1 R_2 C_2 s + R_1 + R_2}{R_1 C_1 R_2 C_2 s^2 + (R_1 C_1 + R_2 C_1 + R_2 C_2) s + 1}$$

can be written $\frac{1}{C_1 s + \frac{R_1 + R_2}{R_1 R_2 C_2}}$

where time constants are

$$\tau_1 = \frac{2 \cdot R_1 C_1}{\left(1 + \frac{C_2}{R_1} + c\right) + \sqrt{\left(1 + \frac{C_2}{R_1} + c\right)^2 - 4 \frac{C_2}{R_1}}}$$

$$\tau_2 = \frac{2 \cdot R_2 C_2}{\left(1 + \frac{C_1}{R_2} + r\right) - \sqrt{\left(1 + \frac{C_1}{R_2} + r\right)^2 - 4 \frac{C_1}{R_2}}}$$

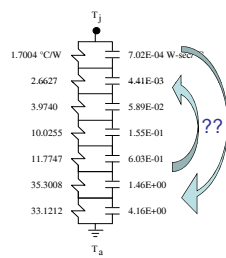
(and defining $r = \frac{R_2}{R_1}$ $c = \frac{C_1}{C_2}$)

r	c	$\frac{\tau_1}{R_1 C_1}$	$\frac{\tau_2}{R_2 C_2}$
100	0.01	0.99	1.01
10	0.1	0.91	1.10
3	1/3	0.73	1.36
1	0.1	0.90	1.11
1	1	0.38	2.62

Interesting (and Important) Implications

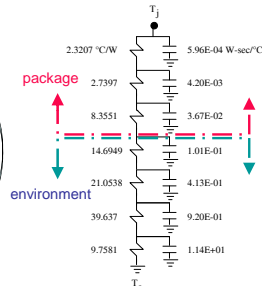
"Foster" ladder

Rungs can be in any order and T_j has identical behavior!
So where do you "split" it?



"Cauer" ladder

Order matters, so a "split" can make good physical sense.



RC Networks in Excel®

Foster ladders of any number of rungs, having simple RC products and associated closed-form transient response, can be easily built and computed using Excel techniques.

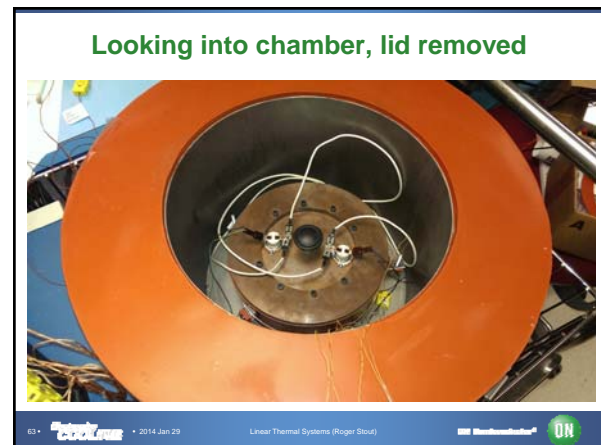
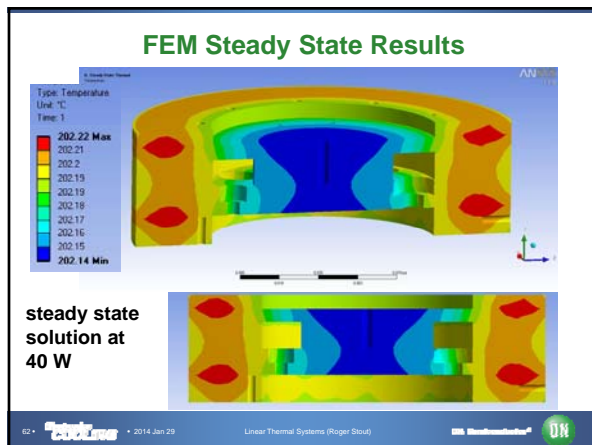
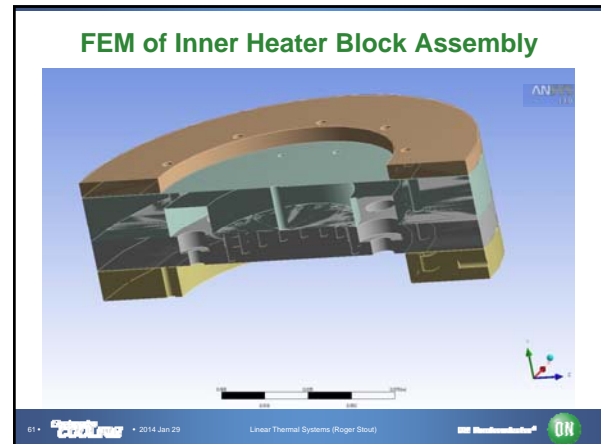
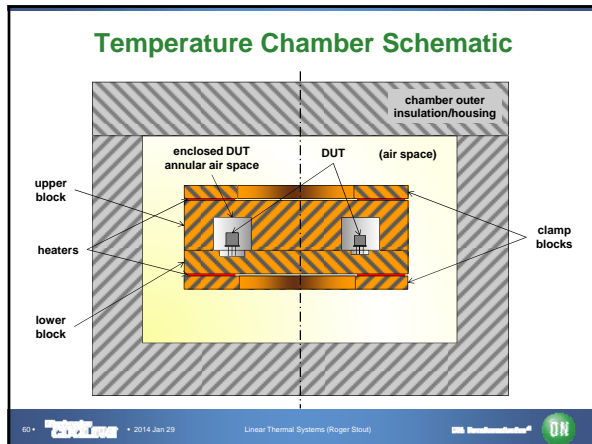
A Foster ladder even can be converted to a Cauer equivalent using Excel techniques. (However, there is no *a priori* guarantee that all R's and C's will be positive!)

Outline

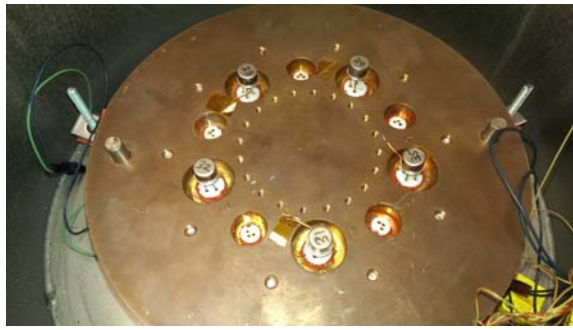
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Temperature Chamber Design Goals

- Test 5 DUT's simultaneously
 - package types: TO18 and TO39
- Range: room temperature to 200 °C
- Hold +/- 0.1 °C uniformity across all DUT's
- Make a 45 °C temperature step with about 0.1 °C accuracy, and be stable within about 15 minutes

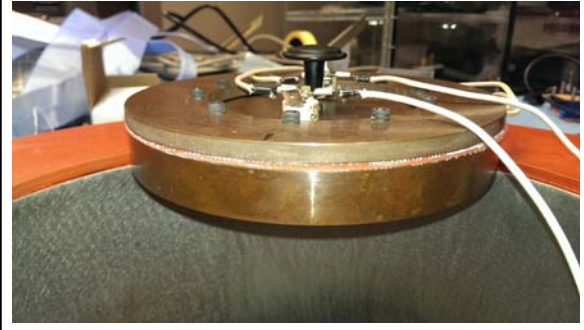


View of DUT cavities in lower heater block



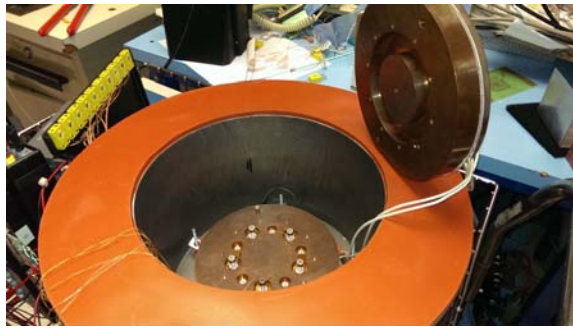
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Side view of upper block and heater clamp



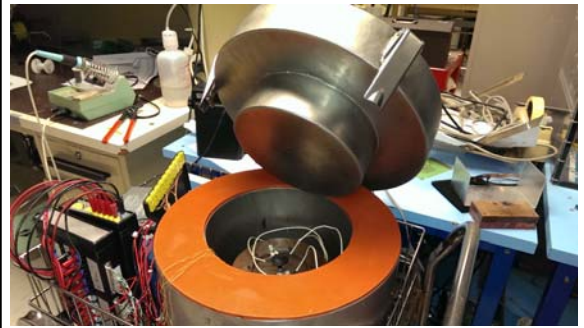
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Another view of opened heater assembly



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Lid ready to be placed onto chamber



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Chamber, temperature controller & scanner



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Poll Question #3

- Roger's high-temperature calibration chamber most resembles:
 - a) A neutrino detector
 - b) A stainless steel hatbox
 - c) A bomb calorimeter
 - d) A phlogiston ambivalizer

(choose all that apply)

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Back-of-the-Envelope Estimates

						convection resistance of inner assembly to air space		
Name of Part	Volume* m³	dens kg/m³	cp J/kg°C	Mth kg	Cth J/°C	surface area m²	0.0669	W/m²/°C
						film coefficient	13	°C/W
Lower Block	2.72E-4	8900	383	2.42	927	R-conv	1.2	°C/W
Upper Block	3.73E-4	8900	383	3.32	1272			
Lower Outer Ring	9.43E-5	8900	383	0.84	321	outside of chamber geometry		
Lower Outer Ring	1.86E-4	8900	383	1.65	633	O.D.	16inch	0.4064 m
Bottom Cover Plate	3.45E-5	8900	383	0.31	118	I.D.	10inch	0.254 m
	9.59E-4		total	8.54	3270	height	16inch	0.4064 m
						wall thickness	0.125inch	0.003175 m
inside of chamber geometry						surface area		
dia	10 inch		0.254 m			top		0.1297 m²
height	8 inch		0.2032 m			bottom		0.1297 m²
wall thickness	0.125 inch		0.003175 m			sides		0.5189 m²
lid/wall overlap	3 inch		0.0762 m			cover/base overlap		0.0790 m²
surface area						total		0.9364 m²
floor		0.0507	m²			volume		0.00207 m³
ceiling		0.0507	m²			steel dens		7850 kg/m³
wall main		0.1621	m²			steel cp		480 J/kg°C
wall overlap		0.0608	m²			mass		23.34 kg
		0.3851	m²					10736 J/°C
total		0.6596	m²			total surface area of outside chamber		0.7783027 m²
volume		0.00122	m³			film coefficient	3.2	W/m²/°C
steel dens		7850	kg/m³			R-conv	0.40	°C/W
steel cp		480	J/kg°C					
mass		9.60	kg					
		4415	J/°C					
convection resistance of inside chamber walls	film coefficient	13	W/m²/°C			conduction resistance of rock wool insulation	thickness	0.0762 m
R-conv	0.20	°C/W					area	0.521 m²
							conductivity	0.055 W/m°C
							R	2.7 °C/W

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More Back-of-the-Envelope (transient) Calculations

- Minimum ramp time

$$\Delta E = C_{th} \Delta T$$

$$time = \frac{\Delta E}{power}$$

step	45 °C
power	230 W
ramp energy	147142 J
ramp time	640 s

- Thermal diffusion time

$$time = \frac{L^2}{\alpha}$$

Cu diffusivity	8.99E-3 s/mm^2	
upper clamp	3 mm	0.08 s
lower clamp	6 mm	0.32 s
block thick	25 mm	5.6 s
block radius	75 mm	51 s

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Even More Back-of-the-Envelope Calculations

- RC time constant of heater block assembly

$$\tau = R_{conv} C_{th}$$

$$= 1.4 \cdot 3300$$

$$= 4600 \text{ s}$$

- RC time constant of outer walls of chamber

$$\tau = R_{conv} C_{th}$$

$$= 0.23 \cdot 15100$$

$$= 3400 \text{ s}$$

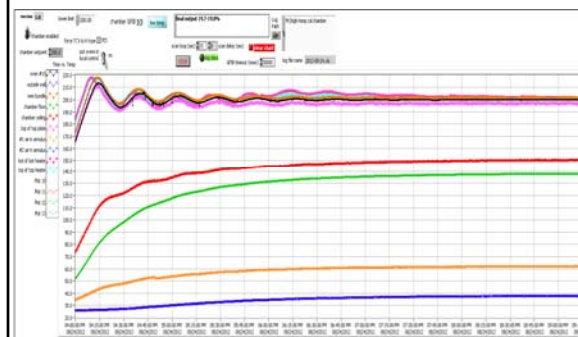
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Commercial PID Controller



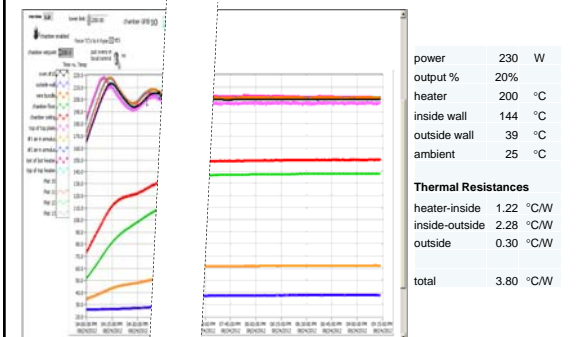
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First "Step Response" Test

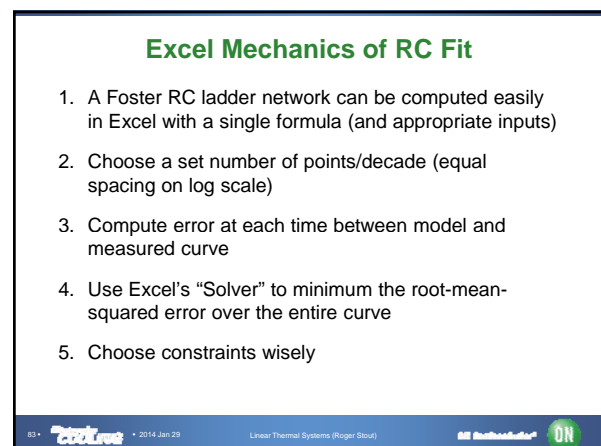
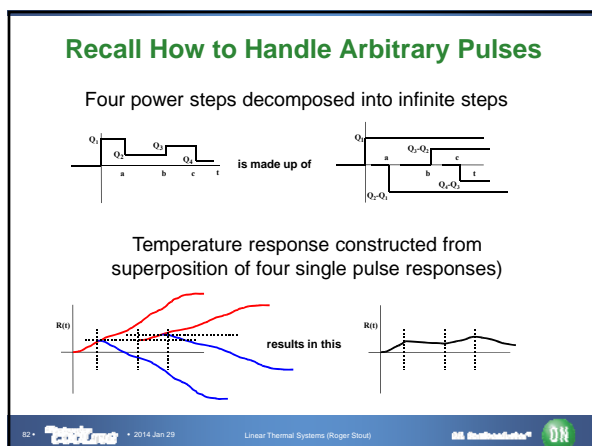
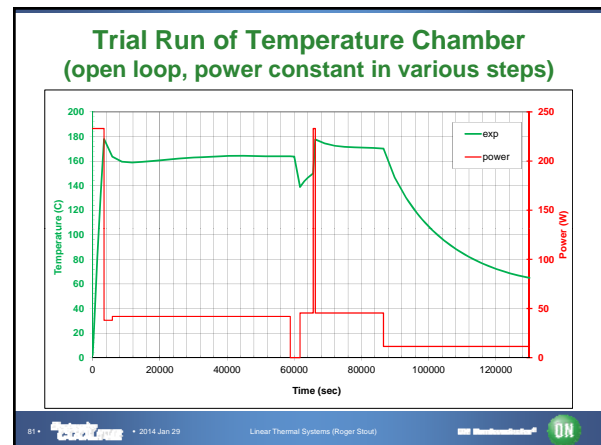
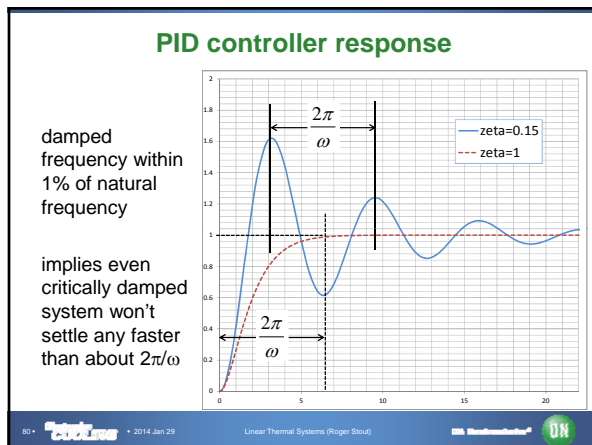
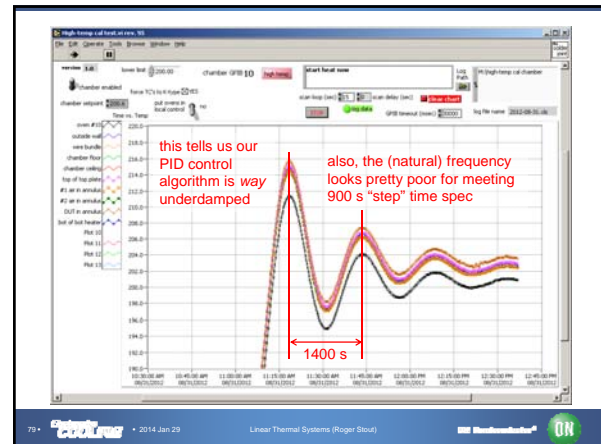
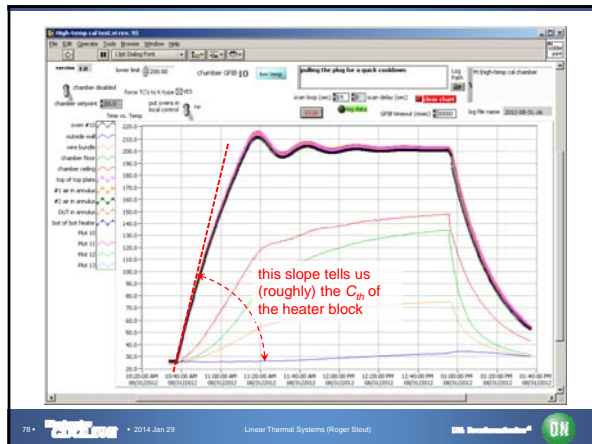


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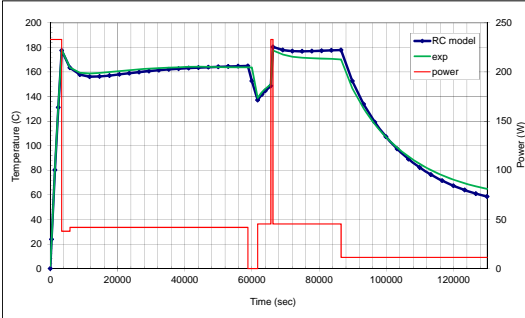
Gain rough steady-state values



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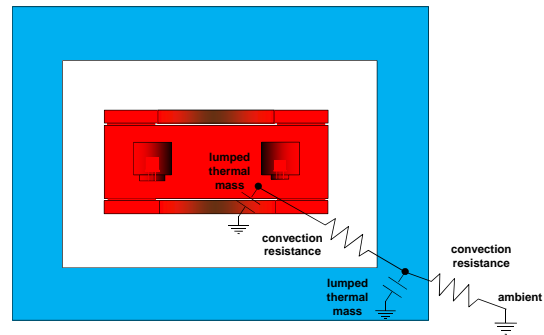


Fitting RC Model to Step Experiment Data



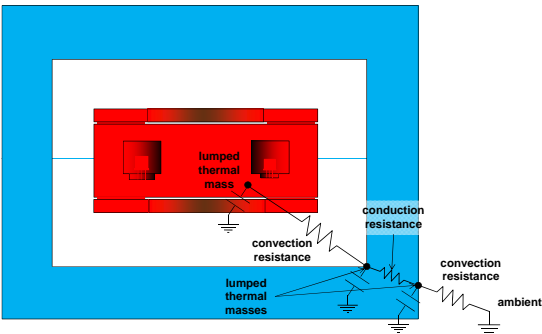
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Very Simple (2-node) Thermal RC Model



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Simple (3-node) Thermal RC Model



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RC Models Fit to Data

2-rung fit (RMSE = 0.000208)

	Foster		Cauer	
Tau	Amp	C's	R's	C's
3850	0.31	12300	2.33	3740
19600	3.65	5380	1.63	5320

Consider the simple RC products:

8730
8650

3-rung fit (RMSE = 0.000250)

	Foster		Cauer	
Tau	Amp	C's	R's	C's
1880	0.002	855000	2.32	3740
3880	0.31	12400	1.47	5100
19600	3.65	5390	0.17	12800

8700
7500
2200

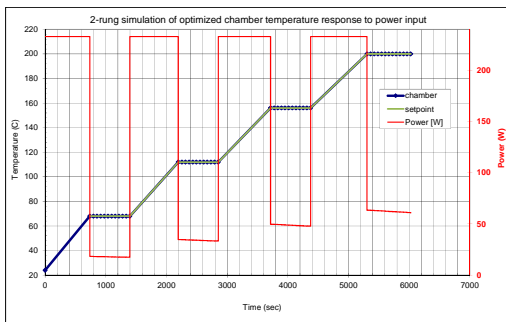
C_{th} -inner heater assy = 3270 J/C

C_{th} -inside walls of outer shell = 4400 J/C

C_{th} -outside wall of outer shell = 10700 J/C

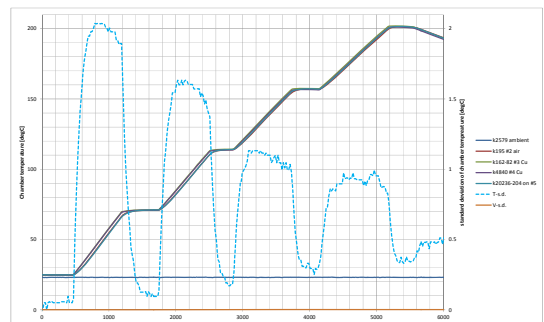
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2-Rung RC Simulation of Optimized Response

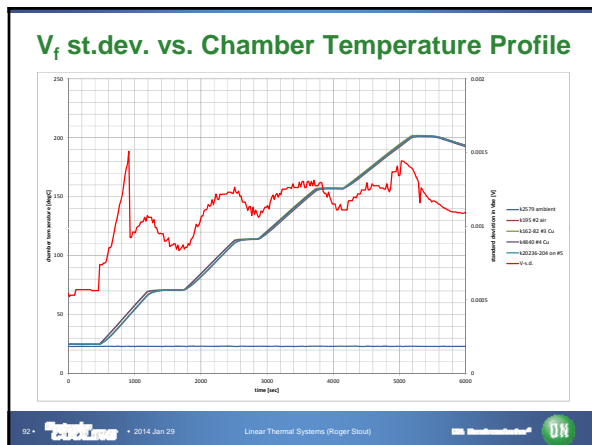
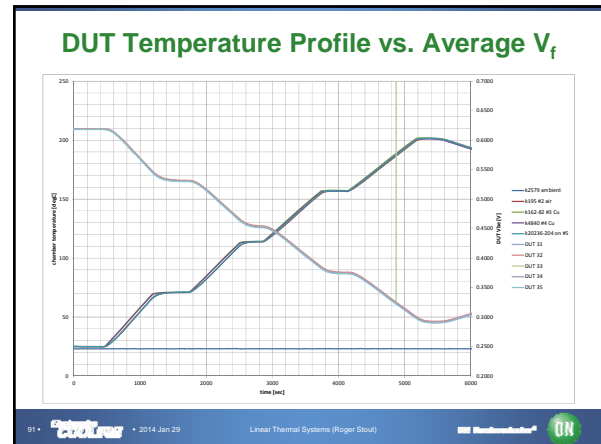
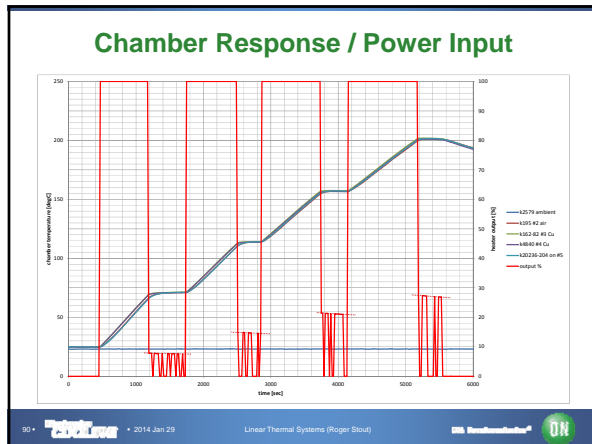


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Actual Open-Loop Chamber Response



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BONUS

If you're interested, and willing to spend another 10-15 minutes ...

How to harness this math in Excel®

Array Formulas and Tables

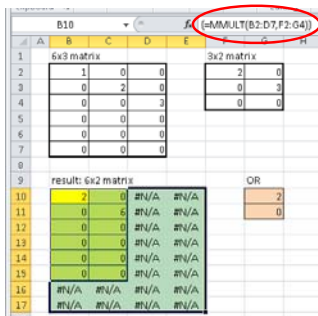
- Array formulas tell Excel
 - apply an operation over a range of cells
 - produce output over (potentially) a range of cells
 - (warning: array formulas applied to AND / OR may surprise you)
- Tables
 - uses a single formula but applies it to a range of values
- With an array formula, you can compute the response of an entire RC ladder in a single formula (for a given time)
- With a carefully designed layout, you can track the response of a train of pulses, one cell for each pulse
- The SUM function can give you the cumulative response of the entire ladder to all pulses (at a given time)
- With a TABLE, you can plot the time history of the whole thing

Some Useful Array and Matrix Functions

- SUM(arguments,...)
 - sums all cells of arguments into single cell result
- MMULT(arg1(m x n) , arg2(n x q))
 - computes matrix multiplication of arg1 by arg2; number of columns of arg1 must number of rows of arg2; result is (m x q) matrix
 - if not entered as array formula, only (1,1) result is returned
- MINVERSE(argument)
 - computes inverse of argument, which must be square matrix
- TRANSPOSE(argument)
 - returns (n x m) matrix for (m x n) argument
- SUMSQ(arguments,...)
 - computes sum of squares of arguments into single cell result

Array Formulas and Matrix Functions

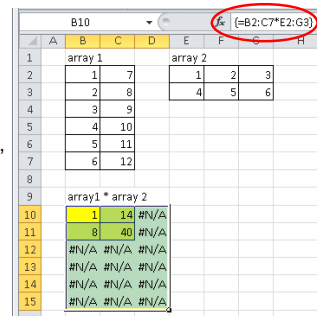
- Array formulas
 - Ctrl-Shift-Enter to create
{braces appear around the formula after entered}
- For example, MMULT
 - yellow area is one formula, but larger than needed
 - beige area is same formula, but only big enough for subset of result



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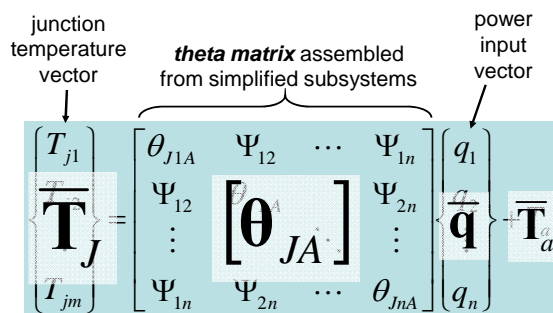
Multiplying Blocks of Cells

- If you just “multiply” two areas (arrays of cells), the size of the result is determined by the intersection of the inputs, and the individual cells are simply the products of the corresponding input values, cell by cell. It’s nothing like MMULT!



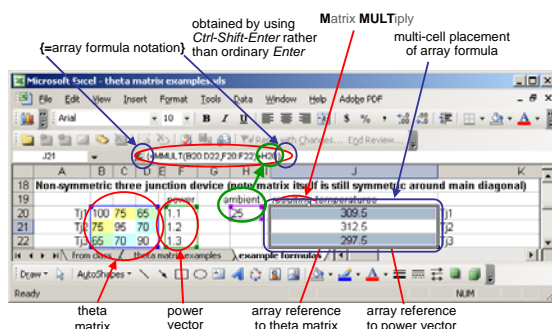
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Multiple independent variables



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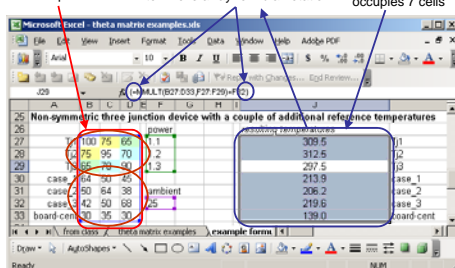
3x3 theta matrix, 3x1 power vector Excel® math



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7x3 theta matrix, 3x1 power vector Excel® math

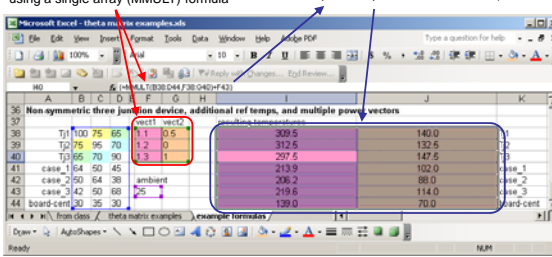
- theta matrix is no longer square – # of rows of power vector must equal
- don't forget to use Ctrl-Shift-Enter to invoke array formula notation
- array formula now occupies 7 cells



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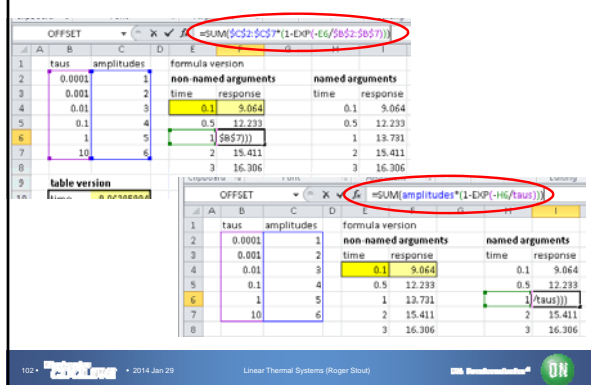
7x3 theta matrix, 3x2 power vector Excel® math

- power “vector” is now a 3x2 array – each column is a different power scenario, yet both are still processed using a single array (MMULT) formula
- the single MMULT array formula now occupies 7 rows and 2 columns (one column for each independent power scenario result)



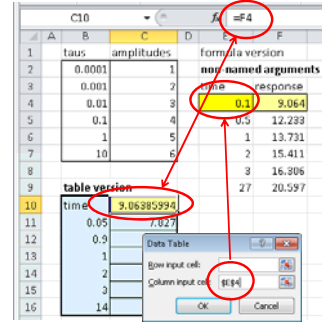
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Using Unnamed and Named Input Values



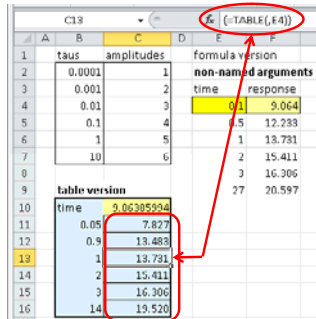
Using Table versus Individual Formulas

- To create table, select entire blue region
- Note light yellow cell can be a formula of its own, or a reference to a formula somewhere else (e.g. cell F4)
- In this example, the "column input cell" is cell E4, because that's the variable argument for the formula in F4

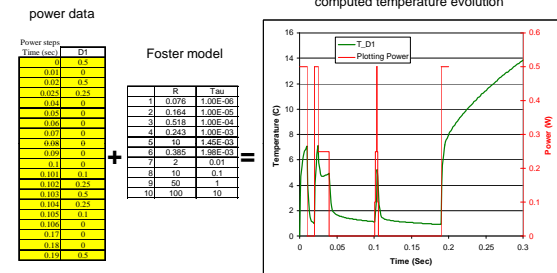


Using Table versus Individual Formulas

- Once table has been created, note that selecting any individual cell below the column formula give you the same $\{=TABLE(E4)\}$ array formula



Putting it Together for a Sequence of Pulses

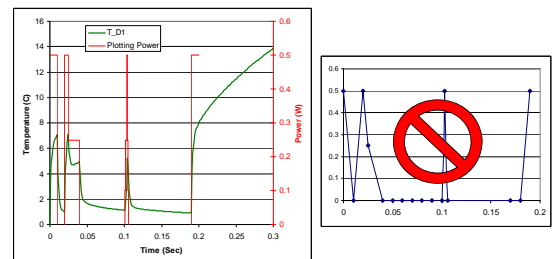


Excel Mechanics of RC Fit

- With an array formula, you can compute the response of an entire Foster RC ladder in a single formula (for a given time)
- With a carefully designed layout, you can track the response of a train of pulses, one cell for each pulse
- The SUM function can give you the cumulative response of the entire ladder to all pulses (at a given time)
- With a table, you can plot the time history of the whole thing
- compute error at selected time points between model and measured curve
- use Excel's "Solver" to minimum the root-mean-squared error over the entire curve

A Note on Graphing the Power Steps

If you want the plot to look like steps, you have to create a special version of the input data table, otherwise you get what looks like ramps (even though it's correctly calculation step responses)



Orders of Magnitude and Rungs

- It is a rare transient curve that cannot be followed very accurately with time constants no closer than about 1 order of magnitude apart. This means that you need only about one rung per decade of transient response.

108 •

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Same Method Can be Applied to Systems with Multiple Heat Sources

- Each heat source has its own Foster description
 - of its own self heating
 - of its interaction with every other location of interest
 - different Foster descriptions don't have to share common time constants
 - it's OK (in fact, it's virtually required) for interaction Foster descriptions to have some negative amplitudes
- The "master" power input table has to introduce a new "step" whenever *any* power input changes, whether you're computing the temperature of that source or simply the effect of that (and every) source in the system; unchanging sources simply have a step of zero

109 •

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110 •

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